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Signed *Andrew George*
Dated 24 December 2003

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19DEC02 E772036-1 C03022
P01/7700 0.00-0229497.3

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(See the notes on the back of this form. You can also get an explanatory leaflet from the Patent Office to help you fill in this form)

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1. Your reference

9890

2. Patent application number

(The Patent Office will fill in this part)

0229497.3

18 DEC 2002

3. Full name, address and postcode of the or of each applicant (*underline all surnames*)

BP CHEMICALS LIMITED
BRITANNIC HOUSE
1 FINSBURY CIRCUS
LONDON
EC2M 7BA
UNITED KINGDOM

Patents ADP number (*if you know it*)

If the applicant is a corporate body, give the country/state of its incorporation

414 189 1502

4. Title of the invention

PROCESS FOR THE PRODUCTION OF OLEFINS

5. Name of your agent (*if you have one*)

SMITH, Julian Philip Howard

"Address for service" in the United Kingdom to which all correspondence should be sent (*including the postcode*)

BP INTERNATIONAL LIMITED
PATENTS & AGREEMENTS
CHERTSEY ROAD
SUNBURY-ON-THAMES
MIDDLESEX
TW16 7LN
UNITED KINGDOM

Patents ADP number (*if you know it*)

4030177002

6. If you are declaring priority from one or more earlier patent applications, give the country and the date of filing of the or of each of these earlier applications and (*if you know it*) the or each application number

| | | |
|---------|--|---|
| Country | Priority application number (<i>if you know it</i>) | Date of filing (<i>day / month / year</i>) |
|---------|--|---|

7. If this application is divided or otherwise derived from an earlier UK application, give the number and the filing date of the earlier application

Number of earlier application

Date of filing
(*day / month / year*)

8. Is a statement of inventorship and of right to grant of a patent required in support of this request? (Answer 'Yes' if:

YES

- a) any applicant named in part 3 is not an inventor, or
- b) there is an inventor who is not named as an applicant, or
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Description 10 / *W*

Claim(s) -

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Statement of inventorship and right to grant of a patent (*Patents Form 7/77*)

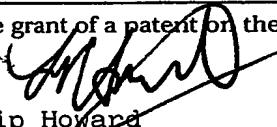
Request for preliminary examination and search (*Patents Form 9/77*)

Request for substantive examination
(*Patents Form 10/77*)

Any other documents
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11.

I/We request the grant of a patent on the basis of this application.

Signature 

SMITH, Julian Philip Howard

Date

18th December 2002

12. Name and daytime telephone number of person to contact in the United Kingdom

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PROCESS FOR THE PRODUCTION OF OLEFINS

The present invention relates to a process for the production of olefins.

Olefins such as ethylene and propylene may be produced by the catalytic dehydrogenation or cracking of a hydrocarbon feed. In this application the term "cracking" will be used to embrace both these chemical reactions. In an auto-thermal cracking process, a hydrocarbon feed is mixed with an oxygen-containing gas and contacted with a catalyst capable of supporting combustion beyond the fuel rich limit of flammability. The hydrocarbon feed is partially combusted and the heat produced is used to drive the cracking reaction.

An example of an auto-thermal cracking process is described in EP 0 332 289.

10 The document describes the use of a paraffinic feed of, for example, ethane, propane and/or butane which is mixed with oxygen and cracked to produce an olefinic mixture. The cracking reaction is endothermic and is carried out at elevated temperatures.

15 The energy required for the cracking reaction is provided by combustion of a part of the feed and the feed may also be preheated but the temperature is limited due to the risk of autoignition.

20 Alternatively the energy required may be provided by a preliminary heat-generating step. In this step a gaseous fuel reacts with oxygen in an exothermic reaction in the presence of a catalyst. The reaction conditions are controlled to ensure that not all of the oxygen is consumed during this process. The thermal energy produced by the reaction heats the unreacted oxygen, thereby providing an additional source of heat to drive the cracking of the hydrocarbon feedstock. This process is described in EP 1 112
241.

However using a catalyst to promote the autothermal cracking process can be problematic because the catalyst is prone to deactivate and consequently needs to be periodically replaced or reactivated. The catalyst may also provide a variable performance. Furthermore the catalyst may cause blockages in the reactor system.

5 It has now been found that autothermal cracking process can be carried out in the substantial absence of a catalyst.

According to the present invention there is provided a process for the production of olefins from a hydrocarbon said process comprising the steps of:

- a) passing a first feed stream comprising gaseous reactants to a first reaction zone
10 wherein said gaseous reactants react exothermically to provide a product stream
- b) producing a mixed feed stream comprising oxygen by passing the product stream produced in step (a) and a second feed stream comprising a hydrocarbon feedstock to a mixing zone and wherein oxygen is passed to the mixing zone via the product stream produced in step (a) and/or via the second feed stream comprising a hydrocarbon
15 feedstock and/or via a third stream comprising an oxygen containing gas
- c) passing the mixed feed stream directly to an essentially adiabatic second reaction zone wherein in the absence of a supported platinum group metal catalyst at least a part of the oxygen is consumed and a stream comprising olefins is produced
- d) cooling the stream comprising olefins exiting the second reaction zone to less than
20 650°C within less than 150milliseconds of formation

and wherein the temperature of the mixed stream is at least 500°C, the mixing zone and the second reaction zone are maintained at a pressure of between 1.5-30bar and the residence time within the mixing zone is less than the autoignition delay for the mixed stream.

25 Additional feed streams comprising at least one from carbon monoxide, carbon dioxide, steam and hydrogen may also be passed to the mixing zone.

Preferably an additional feed stream comprising hydrogen is passed to the mixing zone.

The gaseous reactants in the first feed stream may be any reactants that are capable
30 of reacting exothermically. The heat generated from the exothermic reaction is transferred to the mixed stream via the resultant product stream produced in step (a).

The gaseous reactants may comprise a gaseous fuel and an oxygen-containing gas.

The gaseous fuel may be any gaseous fuel which is capable of reacting with oxygen in an exothermic reaction. Suitable examples include hydrocarbons, such as methane, ethane, propane and butane; with methane being preferred. Other suitable fuels include hydrogen, carbon monoxide, alcohols (eg methanol, ethanol), oxygenates and/or ammonia. Waste fuel streams may also be employed.

5 The oxygen-containing gas may comprise air, oxygen and/or an air/oxygen mixture. The oxygen-containing gas may be mixed with an inert gas such as nitrogen, helium or argon.

10 The first reaction zone may contain a pilot flame or a spark ignition source which is used to initiate the exothermic reaction. Alternatively the first reaction zone may comprise a catalyst.

15 Wherein the first reaction zone contains a catalyst the catalyst usually comprises a supported platinum group metal. Suitable catalyst supports include a range of ceramic and metal supports, with alumina supports being preferred. The support may be in the form of spheres or other granular shapes and may be present as a thin layer or wash coat on another substrate. Preferably the substrate is a continuous multi-channel ceramic structure such as a foam or a regular channelled monolith. In a preferred embodiment a gamma alumina coated alpha alumina. Alternatively zirconia or a gamma alumina coated lithium aluminium silicate foam support may be employed.

20 The first feed stream may be passed to the first reaction zone at a temperature of between 600 and 1400°C, preferably between 700 and 1200° C and most preferably between 950 and 1100°C.

25 The first reaction zone may be maintained at any suitable pressure e.g. atmospheric pressure. Usually the first reaction zone is maintained at a pressure of from 1.5 to 50 bara, for example between 1.8 to 50 bara, preferably between 5-50bara, most preferably between 5 to 30 bara and advantageously between 10-30bara. It will be understood that the precise pressures employed will vary depending on the specific reaction conditions and gaseous reactants employed.

30 The first feed stream is usually introduced into the first reaction zone at a gas hourly space velocity GHSV of greater than $10,000 \text{ h}^{-1}$, preferably above $100,000 \text{ h}^{-1}$ and most preferably greater than $300,000 \text{ h}^{-1}$. It will be understood that the optimum gas hourly space time velocity will depend upon the pressure and nature of the feed

composition.

In one embodiment of the invention the product stream produced in step (a) may comprise oxygen. Consequently the first feed stream may comprise a gaseous fuel and an oxygen-containing gas which may be passed to the first reaction zone wherein a 5 product stream comprising unreacted oxygen is produced. The product stream may then be passed to the mixing zone to provide the mixed feed stream comprising oxygen.

When the product stream comprising unreacted oxygen is produced the first feed stream comprising a gaseous fuel and an oxygen containing gas is preferably fuel-rich with a fuel to oxygen ratio above the stoichiometric ratio required for complete 10 combustion. For example, the fuel to oxygen ratio in the feed may be 1.5 to 4 times, preferably 3 times the stoichiometric ratio required for complete combustion to carbon dioxide to water.

The gaseous fuel and oxygen-containing gas may be contacted in the first reaction zone under reaction conditions which are controlled to ensure that some of the oxygen 15 in the first feed stream remains unreacted. The thermal energy produced in step (a) heats the unreacted oxygen thereby providing part of the heat necessary for cracking the hydrocarbon feedstock in step (c).

The reaction between the gaseous fuel and oxygen-containing gas may be a combustion reaction. Accordingly gaseous fuel in the first feed stream may react with 20 oxygen to produce a product stream comprising oxides (eg carbon oxides) and water. In such an embodiment and wherein the first reaction zone contains a catalyst a combustion catalyst is employed. Suitable combustion catalysts include Group VIII metals such as platinum and/or palladium. The catalyst may comprise 0.1 to 5 wt% and preferably 0.25 to 3 wt% of metal. It will be understood that the metal loadings of the 25 catalyst may be selected to ensure that not all the oxygen in the first feed stream is consumed in step (a).

In an alternative embodiment the gaseous fuel of the first feed stream reacts with the oxygen-containing gas to produce synthesis gas. In this embodiment a first feed stream comprising a hydrocarbon (eg methane) is employed which reacts with oxygen to 30 produce carbon monoxide and hydrogen. These gaseous products may react exothermically, for example with oxygen, thereby providing a further source of heat to drive the cracking reaction in step (c). In this embodiment, and wherein a catalyst is

employed the catalyst is one which is capable of supporting a synthesis gas production reaction. Suitable catalysts comprise rhodium, platinum, palladium, nickel or mixtures thereof. Preferably a rhodium catalyst is used. The catalyst may comprise 0.1 to 5 wt% and preferably 0.25 to 3 wt%, of metal. As with combustion catalysts, the metal

5 loadings of the catalyst may be varied to ensure that not all the oxygen in the first feed stream is consumed in step (a).

In a further embodiment a gaseous fuel is reacted with an oxygen-containing gas in a combustion reaction and another gaseous fuel (which may or may not be the same as the first gaseous fuel) is reacted with an oxygen-containing gas to produce synthesis

10 gas. Both these reactions are exothermic and may provide part of the heat for driving the subsequent cracking reaction in step (c). In at least one of these reactions, however, not all of the oxygen-containing gas employed is consumed. At least part of this unreacted oxygen is consumed in step (c) to produce the olefin product of the present invention.

The product stream produced from step (a) is usually passed to the mixing zone at

15 a temperature of between 900 and 1300°C, preferably between 950 and 1250°C, and most preferably between 1000 and 1200°C.

In another embodiment of the invention the second feed stream may comprise oxygen. The second feed stream comprising oxygen may then be mixed with the product stream produced in step (a) to provide the mixed feed stream comprising oxygen.

20 The second feed stream may comprise any suitable hydrocarbon and may optionally comprise an oxygen containing gas. For example, gaseous hydrocarbons, heavy hydrocarbons or mixtures thereof may be employed. Suitable gaseous hydrocarbons include ethane, propane, butane and mixtures thereof. Suitable heavy hydrocarbons include naptha, gas oil, vacuum gas oil, refinery residues, atmospheric

25 residues, vacuum residues and crude and fuel oils. Additional feed components such as hydrogen, nitrogen, carbon monoxide, carbon dioxide and steam may also be included in the second feed stream. Hydrogen and/or carbon monoxide may react with the oxygen present to produce additional heat for driving the cracking process. In the second feed stream, a gaseous hydrocarbon may be alternated with a heavy hydrocarbon, as the

30 hydrocarbon feed stock.

The second feed stream is usually heated to a temperature of 200°C to 600°C, and preferably to 300°C to 500°C.

The second feed stream is introduced at a gas hourly space velocity of greater than 10,000 h⁻¹, preferably above 20,000 h⁻¹ and most preferably greater than 100,000 h⁻¹. It will be understood, however, that the optimum gas hourly space time velocity will depend upon the pressure and nature of the feed composition.

5 The second feed stream comprising a hydrocarbon feedstock and optionally oxygen is contacted with the product stream produced in step (a) which may or may not contain unreacted oxygen in a mixing zone wherein a mixed feed stream comprising oxygen is produced.

In yet another embodiment of the invention a third feed stream comprising an 10 oxygen containing gas may be fed to the mixing zone to provide the mixed feed stream comprising oxygen. The oxygen containing gas may be any oxygen containing gas as herein described above.

The temperature of the mixed feed stream is at least 500°C, preferably at least 600°C and most preferably at least 700°C.

15 The mixing zone is maintained at a pressure of between 1.5 to 50 bara, for example between 1.8 to 50 bara, preferably between 5-50bara, most preferably between 5 to 30 bara and advantageously between 10-30bara.

The mixing zone is usually a mixing channel that passes directly into the second 20 reaction zone. The residence time of the mixed feed stream in the mixing zone is less than the autoignition delay of the mixed feed stream. This ensures that the production of olefins does not commence until the mixed feed stream enters the second reaction zone.

Typically the residence time within the mixing zone is less than 100 milliseconds, 25 preferably less than 50milliseconds, most preferably less than 10milliseconds and advantageously less than 5 milliseconds.

Preferably the mixed feed stream is passed through the mixing zone and into the 30 into the second reaction zone at a velocity of greater than 1 m/s, preferably greater than 3 m/s. These velocities are sufficiently high to prevent flashback into the first reaction zone.

The second reaction zone is essentially adiabatic so that reaction therein occurs without heat entering or leaving the reaction zone. This is achieved by insulating the 35 second reaction zone.

The hydrocarbon feed in the second feed stream may be cracked into olefins such

as ethene, propene, butene and pentene or a mixtures thereof.

The cracking reaction may be suitably carried out at a temperature of between 600 and 1200°C , preferably between 850 and 1050 °C and most preferably, between 900 and 1000 °C. It will be understood that the optimum temperature will depend upon the
5 feed mixture and operating pressure.

The cracking reaction is carried out in the second reaction zone at a pressure of between 1.5 to 50 bara, for example, between 1.8 to 50 bara, preferably between 5-50bara, most preferably between 5 to 30 bara and advantageously between 10-30bara. It will be understood that the precise pressures employed will vary depending on the
10 specific reaction conditions and gaseous fuels employed.

The second reaction zone does not contain a supported platinum group metal catalyst. Preferably the second reaction zone does not contain any catalytic material that is capable of supporting combustion beyond the normal fuel rich limit of flammability. Most preferably the second reaction zone does not contain any material that would
15 exhibit any substantial catalytic activity.

The second reaction zone may contain a stabiliser and/or packing materials such porcelain, ceramics, alumina and/or silica that do not exhibit any substantial catalytic activity.

In a preferred embodiment the second reaction zone may contain a grid(s), a
20 perforated plate(s), and/or a baffle plate(s).

In another preferred embodiment of the invention the second reaction vessel comprises a heated gauze which encourages the reaction to occur at a particular location within the vessel.

In a further embodiment the second reaction zone is essentially empty.

25 In a preferred embodiment of the invention the residence time within the second reaction zone is sufficient to ensure that substantially all the oxygen is consumed.

Typically the residence time within the second reaction zone is less than 100milliseconds, preferably less than 50milliseconds and advantageously less than 10milliseconds.

30 After the cracking reaction the products are quenched as they emerge from the second reaction zone such that the temperature is reduced to less than 650°C within less than 150milliseconds of formation.

Wherein the pressure of the second reaction zone is maintained at a pressure of between 1.5-2.0bara usually the products are quenched and the temperature reduced to less than 650°C within 100-150milliseconds of formation.

5 Wherein the pressure of the second reaction zone is maintained at a pressure of between 2.0-5.0bara usually the products are quenched and the temperature reduced to less than 650°C within 50-100milliseconds of formation.

Wherein the pressure of the second reaction zone is maintained at a pressure of between 5.0-10.0bara usually the products are quenched and the temperature reduced to less than 650°C within less than 50milliseconds of formation.

10 Wherein the pressure of the second reaction zone is maintained at a pressure of between 10.0-20.0bara usually the products are quenched and the temperature reduced to less than 650°C within 20milliseconds of formation.

15 Finally wherein the pressure of the second reaction zone is maintained at a pressure of greater than 20.0bara usually the products are quenched and the temperature reduced to less than 650°C within 10milliseconds of formation.

This avoids further reactions taking place and maintains a high olefin selectivity.

The products may be quenched using rapid heat exchangers of the type familiar in steam cracking technology. Additionally or alternatively, a direct quench may be employed. Suitable quenching fluids include water and hydrocarbons such as ethane or naphtha.

The present invention usually provides a percentage conversion of hydrocarbon of greater than 40%, preferably greater than 50%, and most preferably greater than 60%.

Furthermore the present invention usually provides a selectivity towards olefins of greater than 20%, preferably greater than 30%, and most preferably greater than 50%.

25 Any coke produced in the process of the present invention may be removed by mechanical means, or using one of the decoking methods described in EP 0 709 446, incorporated herein by reference.

Example 1

A first feed stream comprising the gaseous reactants methane and oxygen was passed to the first reaction zone comprising a promoted palladium catalyst at a temperature of 400°C wherein gaseous reactants exothermically reacted to provide a synthesis gas product stream. The first reaction zone was maintained at a pressure of 1.8

bar.

The product stream comprising hydrogen, carbon monoxide, carbon dioxide, and water was passed to the mixing zone at a flow rate of 12.54g/min wherein the hydrogen flow rate was 1.31g/min, the carbon monoxide flow rate was 9.48g/min, the carbon dioxide flow rate was 0.75g/min and the water vapour flow rate was 1.00g/min. The temperature of the product stream was 1200°C.

A second feed stream comprising ethane and oxygen was passed to the mixing zone at a flow rate of 24.97g/min wherein the ethane flow rate was 18.80g/min and the oxygen flow rate was 6.17g/min. The temperature of the second feed stream was 450°C.

10 The residence time in mixing channel was less than 5ms.

The mixed feed stream with a combined temperature of 610°C was passed directly to the second reaction zone wherein in the absence of a catalyst the oxygen was consumed and the ethane was converted to ethylene. The second reaction zone was also maintained at a pressure of 1.8bar.

15 The product stream exiting the second reaction zone at a temperature of 770°C was cooled using a water quench to 600°C within less than 50milliseconds of formation.

The % conversion of ethane was measured a 68.1% and the selectivity towards ethylene was measured at 77.2%.

Example 2

20 A first feed stream comprising the gaseous reactants methane and oxygen was passed to the first reaction zone comprising a promoted palladium catalyst at a temperature of 300°C and at a flow rate of 41.0g/min wherein the flow rate of methane was 18.4g/min and the flow arte of oxygen was 22.6g/min. The gaseous reactants exothermically reacted to provide a synthesis gas product stream. The first reaction zone 25 was maintained at a pressure of 20 bar.

The product stream comprising hydrogen, carbon monoxide, carbon dioxide, and water was passed to the mixing zone at a flow rate of 40.99g/min wherein the hydrogen flow rate was 4.30g/min, the carbon monoxide flow rate was 29.32g/min, the carbon dioxide flow rate was 4.61g/min and the water vapour flow rate was 2.76g/min. The 30 temperature of the product stream was 1200°C.

A second feed stream comprising ethane and oxygen was passed to the mixing zone at a flow rate of 125.37g/min wherein the ethane flow rate was 100g/min and the

oxygen flow rate was 25.37g/min. The temperature of the second feed stream was 250°C.

The residence time in mixing channel was less than 5ms.

5 The mixed feed stream with a combined temperature of 600°C was passed directly to the second reaction zone wherein in the absence of a catalyst the oxygen was consumed and a the ethane was converted to ethylene. The second reaction zone was also maintained at a pressure of 20bar.

The product stream exiting the second reaction zone at a temperature of 800°C was cooled using a water quench to 600°C within less than 20milliseconds of formation.

10 The % conversion of ethane was measured a 61.4% and the selectivity towards ethylene was measured at 32.06%.

Comparative Example

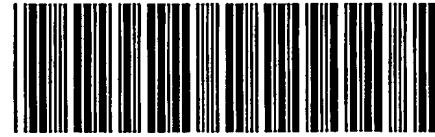
A mixed feed stream comprising hydrogen, oxygen and ethane was passed to the mixing zone at a flow rate of 24.81g/min wherein the hydrogen flow rate was 0.70g/min
15 the ethane flow rate was 18.53g/min and the oxygen flow rate was 5.58g/min. The temperature of the feed stream was 450°C.

The mixed feed stream was passed directly to reaction zone comprising a supported platinum group metal catalyst wherein oxygen was consumed and a the ethane was converted to ethylene. The reaction zone was also at a pressure of 1.8bara.
20 The product stream exiting the reaction zone at a temperature was cooled using a water quench to 600°C within less than 50milliseconds of formation.

The % conversion of ethane was measured a 67.6% and the selectivity towards ethylene was measured at 79.0%.

It can be seen from the above examples that an autothermal cracking reaction can
25 be operated in the absence of a catalyst and achieve a high hydrocarbon conversion and a high selectivity towards olefins.

PCT Application
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